## Specification for the CPI Component Data File Format Version 2.0 Revised: 25/02/2011

## Introduction

This document provides a specification for the University of Manchester Centre for Process Integration (CPI) Data File (CMP File) format. The CMP file format is a proprietary format, containing a list of components and physical properties, together with the parameters required to calculate those properties.

The physical property algorithms themselves are encoded into the CPI's suite of process integration software. The purpose of the CMP file is to provide a consistent mechanism whereby the components and parameters can be imported into CPI's software.

A CMP file contains:

- A list of chemical components
- A list of physical properties (e.g. enthalpy, vapour pressure)
- A list of methods, used to calculate the physical properties
- A list of parameters which are required for calculation of the property, using the specified method

CMP files are currently created using Component Editor (CmpEdit), a file editor supplied with CPI's software.

The purpose of this document is to provide sufficient information to enable third parties to produce CMP files which are compatible CPI's software. In particular it enables the writing of macros which automatically export the data from commercial simulators.

## Basic Principles

The basic properties of the CMP file are:-

- Free-format ASCII
- Case insensitive
- Order insensitive (within each section)

The file consists of the following three sections

- Headers: This must be the first section in the file, and contains the version number of the data file, and optional information regarding the source of the data.
- Counters: This must precede the Data section, and provides summary information regarding the number of components and properties that follow in the file. The start of the Counters section is identified in the file by the single line:


## [COUNTERS]

- Data Section: The Data section must follow the Counters section, and contains all the information and parameters relating to the components and properties introduced in the Counters section. The start of the Data section is identified in the file by the single line:


## [DATA]

Within each section, information is supplied in the form:

```
Item_Name = value_1, value_2, value_3..., value_n
```

Where Item_Name is a unique keyword, followed by a list of values separated by commas. The values may be of type integer, real or character, and must all be on the same line as the keyword. The number and type of values associated with each keyword is fixed, and defined below.

Comments my be freely used anywhere within the file by including "[\#\#\#" or "!" as the first characters on the line, e.g.
[\#\#\# this is a comment]
! This is also a comment
In-line comments may be included with the ";" character. Any text following the ";" character is ignored, for the rest of the line, e.g.

$$
\text { NUM_Components }=5 \quad \text {; Comment }-5 \text { components in file }
$$

## Keywords

The following is a complete list of the keywords recognised for use in a CMP file. Each keyword must appear in its respective section (Headers, Counters or Data). Any keyword that is not in the correct section, or is not recognised, will be ignored without affecting the validity of the rest of the file.

Each keyword is specified as follows
KeyWord = <value_1>, <value_2>, ... <value_n>

The type of each value is indicated

$$
\begin{array}{ll}
<n> & =\text { Integer } \\
<\mathrm{r}> & =\text { Real }
\end{array}
$$

<string> $\quad=$ Character string

## Headers Section

The first line of the header must consist of the current version number, followed by optional reference information, for example:

## 2.0 [UMIST CMP Data File Version Number 02/11/1998 10:34:00]

The CMP file is currently at version 2.0
The following optional keywords may be included in the headers, but are not required:
Inf_Program_Name = <string>
where $<$ String $>$ is the source of the data
Inf_Program_Version = <n>
where $<\mathrm{n}>$ is the version number of the data source

## Inf_Program_Build_Date = <n> <br> where $<\mathrm{n}>$ is the date of file creation

## Counters Section Section

The following keywords and associated values are required in the Counters section of the file. Note that all counter keywords begin with the prefix NUM_

NUM_Components = <n>
Number of components
$<\mathrm{n}>$ is the number of components present in the file

## NUM_Properties = <n>

Number of properties
<n> is the number of properties within the file. See Appendix A for a full list of available properties.

NUM_CompID = <n1>, <n2>
Component ID number
$<\mathrm{n} 1>$ is the ordinal number of the component within the file $<$ n2> is a unique identification number (ID number) for the component. Throughout the entire file each component is referenced by its ID number.

NUM_PropID = <n1>, <n2>
Property reference number
$<\mathrm{n} 1>$ is the ordinal number of the property within the file
$<\mathrm{n} 2>$ is the reference number of the component. See Appendix A for a list of property reference numbers.

The following keywords and associated values are required in the Data section of the file. Note that all counter keywords begin with the prefix PPD_. If all of the values associated with a particular keyword are equal to 0.0 , the keyword may be omitted from the file.

PPD_LongName = <n>, <string>
Component long name
$<\mathrm{n}>$ is the ID number of a component
<string> is a long name for the component. The name may be up to 40 characters long
PPD_ShortName = <n>, <string>
Component short name
$<\mathrm{n}>$ is the ID number of a component
<string> is a short name (e.g. formula) for the component. The name may be up to 15 characters long

PPD_PropertyMethod = <n1>, <n2>
Method used to calculate a property
$<\mathrm{n} 1>$ is the reference number of the property
<n2> is the method number for the property. See Appendix A for a list of property reference and method numbers.

Critical data for a component
$<\mathrm{n}>$ is the ID number of the component
$<\mathrm{rl}>$ is the molecular weight, MolWt, $(\mathrm{g} / \mathrm{mol})$
$<\mathrm{r} 2>$ is the normal freezing point at 1 atmosphere, Tfp, (Kelvin)
$<\mathrm{r} 3>$ is the normal boiling point at 1 atmosphere, Tb, (Kelvin)
$<\mathrm{r} 4>$ is the critical temperature, Tc, (K)
$<\mathrm{r} 5>$ is the critical pressure, Pc, (Bar)
$<r 6>$ is the critical volume, $\mathrm{Vc},\left(\mathrm{cm}^{3} / \mathrm{mole}\right)$
$<\mathrm{r} 7>$ is the critical compressibility factor, $\mathrm{Zc}(\mathrm{PcVc} / \mathrm{RTc})$
$<$ r8> is Pitzer's acentric factor
$<\mathrm{r} 9>$ is the dipole moment, (debyes)
PPD_CriticalDat2 = <n>, <r1>, <r2>, <r3>, <r4>, <r5>, <r6>, <r7>, <r8>, <r9> Critical data for a component
c PURE_PROP_DN = density at std condition $\left(\mathrm{kg} / \mathrm{m}^{\wedge} 3\right)-$ maybe
$<\mathrm{n}>$ is the ID number of the component
$<\mathrm{r} 1>$ is the solubility, Sl (????)
$<\mathrm{r} 2>$ is Molar Volume, Mv, (cm3/mol)
$<\mathrm{r} 3>$ is the Non-condensable flag , (0/1)
$<\mathrm{r} 4>$ is the density at standard condition, $\mathrm{Dn},\left(\mathrm{kg} / \mathrm{m}^{\wedge} 3\right)$
$<r 5>$ reserved for future use
$<$ r6> reserved for future use
$<r 7>$ reserved for future use
$<$ r8> reserved for future use
$<$ r9> reserved for future use

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PPD_PropParam = <n1>, <n2>, <n3>, <r>
Parameters for a component/property pair. The number of parameters for each component/property pair depends on the method being used to calculate the property. $<\mathrm{n} 1>$ is the reference number of the property
$<\mathrm{n} 2>$ is the ID number of the component
$<$ n3> is the parameter number
$<\mathrm{r}>$ is the value of the parameter. See Appendix A for a list of parameters required for
each property/method combination

PPD_InterParam = <n1>, <n2>, <n3>, <r1>, <r2>
Binary interaction parameters for a component pair (only required when the Activity Coefficients property is present)
$<\mathrm{n} 1>$ is the ID number of the first component in the pair
$<$ n2> is the ID number of the second component in the pair
$<$ n3> is the number of binary matrix. (Refer to Appendix A for details of which binary matrices are required for each Activity Model.)
$<\mathrm{rl}>$ is the value of the interaction parameter for component pair <n1>, <n2>
$<\mathrm{r} 2>$ is the value of the interaction parameter for component pair <n2>,<n1>
Example:
PPD_InterParam =77, 170, 1, 904.77, -14.583
Indicates that:
$\mathrm{A}_{\mathrm{i}, \mathrm{j}}=904.77$
$\mathrm{A}_{\mathrm{j}, \mathrm{i}}=-14.583$
i is the component with ID number 77
j is the component with ID number 170

## Appendix A: Physical Properties and Methods

This appendix describes the primary physical property routines and methods that are available in the CPI's software.

Where a property/method pair requires additional parameters, the form of the equation used is supplied. If a property requires no additional parameters, the form of the equation is not required to produce a CMP file, and is not supplied. This keeps the amount of information supplied to a bare minimum.

The available property list currently comprises three core properties (enthalpy, vapour pressure and equation of state), an activity model, and several further optional properties. The optional properties are only required in a small class of calculations, and are not included in this version of the specification.

A CMP file must always contain the three core properties as a minimum. The activity model is optional. If the activity model is present it will be used for calculating liquid phase properties, with the selected equation of state being used for vapour phase calculations only.

The properties and methods are summarised in the following table

| Property <br> Name | Reference Number | Available Methods | Require <br> d |
| :---: | :---: | :---: | :---: |
| Enthalpy | 2 | 1: Reid, Prausnitz, Poling <br> 2: DIPPR <br> 3. Hysys-Tabular <br> 4. Lee-Kesler | Yes |
| Vapour Pressure | 3 | $$ | Yes |
| Equation of State | 11 | ```1: Ideal Gas (Raoult's Law) Peng-Robinson Soave-Redlich-Kwong (SRK) 4: Grayson-Streed``` | Yes |
| Activity Model | 9 | 1: Wilson <br> 2: NRTL <br> 3: UNIQUAC <br> 4: Extended NRTL <br> (AspenTech) | No |

## Enthalpy

## Method 1: Reid-Prausnitz-Poling

This method uses a standard third order polynomial to calculate the heat capacities, and integrates with respect to temperature to calculate the enthalpies.

The equation used to calculate the heat capacities is:

$$
C p=A+B T+C T^{2}+D T^{3}
$$

Where $C p=$ heat capacity of the ideal gas, $\mathrm{J} /(\mathrm{mol} . \mathrm{K})$
$T=$ Temperature, K
The parameters required on the respective PPD_PropParam keyword are:

| Parameter <br> Number | Parameter Name | Parameter Symbol/Description |  |
| :---: | :---: | :--- | :---: |
| 1 | CPVAP A | $A$ |  |
| 2 | CPVAP B | $B$ |  |
| 3 | CPVAP C | $C$ |  |
| 4 | CPVAP D | $D$ |  |

Ref. The Properties of Gases and Liquids, 4th Edition, Reid, Prausnitz and Poling, p. 657

## Method 2: DIPPR

This method uses the DIPPR ideal gas heat capacity equation, and integrates with respect to temperature to calculate the enthalpies.

The equation used to calculate the heat capacities is:

$$
C p=C_{1}+C_{2}\left(\frac{C_{3} / T}{\sinh \left(C_{3} / T\right)}\right)^{2}+C_{4}\left(\frac{C_{5} / T}{\cosh \left(C_{5} / T\right)}\right)^{2} \text { for } T_{\min } \leq T \leq T_{\max }
$$

Where $C p=$ heat capacity of the ideal gas, $\mathrm{J} /(\mathrm{mol} . \mathrm{K})$
$T=$ Temperature, K
The parameters required on the respective PPD_PropParam keyword are:

| Parameter <br> Number | Parameter <br> Name | Parameter Symbo/Description |
| :---: | :---: | :--- |
| 1 | CPVAP A | $\mathrm{C}_{1}$ |
| 2 | CPVAP B | $\mathrm{C}_{2}$ |
| 3 | CPVAP C | $\mathrm{C}_{3}$ |
| 4 | CPVAP D | $\mathrm{C}_{4}$ |
| 5 | CPVAP E | $\mathrm{C}_{5}$ |
| 6 | Tmin | Lower temperature limit (K) |


| 7 | Tmax | Upper temperature limit (K) |
| :--- | :--- | :--- |

Ref AspenTech User Guide V10.2, Physical Property Methods and Models, p3-109

## Method 3: Hysys Tabular

## Method 4: Les-Kesler

This method uses a standard third order polynomial to calculate the enthalpies, and differentiates with respect to temperature to calculate the heat capacities

The equation used to calculate the enthalpies is:
$\mathrm{H}=\mathrm{A}+\mathrm{B}^{*} \mathrm{~T}+\mathrm{C}^{*}\left(\mathrm{~T}^{2}\right)+\mathrm{D}^{*}\left(\mathrm{~T}^{3}\right)+\mathrm{E}^{*}\left(\mathrm{~T}^{4}\right)$
Where:-
$\mathrm{H}=$ Enthalpy of ideal gas at temperature $\mathrm{T}[\mathrm{kJ} / \mathrm{kg}]$
$\mathrm{T}=$ Temperature [K]

The parameters required on the respective PPD_PropParam keyword are:

| Parameter <br> Number | Parameter Name | Parameter Symbol/Description |
| :---: | :---: | :--- |
| 1 | CPVAP A | A |
| 2 | CPVAP B | $B$ |
| 3 | CPVAP C | C |
| 4 | CPVAP D | $D$ |
| 5 | CPVAP E | $E$ |

( Ref: HYSIM Ver.2.10 User's Guide, 1993, pp.5-29)

## Vapour Pressure

## Method 1: Reid-Prausnitz-Poling

This method uses one of three equations to calculate vapour pressure, as follows:

$$
\begin{array}{ll}
\text { Eqn (1) } & \ln (P v p / P c)=(1-x)^{-1}\left[(V P A) x+(V P B) x^{1.5}+(V P C) x^{3}+(V P D) x^{6}\right] \\
& x=1-T / T c \\
\text { Eqn (2) } & \ln (P v p)=V P A-(V P B) / T+(V P C) \ln T+(V P D)(P v p) T^{2} \\
\text { Eqn (3) } & \ln (P v p)=V P A-(V P B) /(T+(V P C))
\end{array}
$$

Where $P v p=$ Vapour pressure, bars
$P c=$ Critical pressure, bars
$T c=$ Critical temperature, K
$T=$ Temperature, K

The parameters required on the respective PPD_PropParam keyword are:

| Parameter <br> Number | Parameter <br> Name | Parameter Symbol/Description |
| :---: | :---: | :--- |
| 1 | Eqn. No. | Equation number |
| 2 | VP A | $V P A$ |
| 3 | VP B | $V P B$ |
| 4 | VP C | $V P C$ |
| 5 | VP D | $V P D$ |
| 6 | Tmin | Lower temperature limit (K) |
| 7 | Tmax | Upper temperature limit (K) |

Ref. The Properties of Gases and Liquids, 4th Edition, Reid, Prausnitz and Poling, p. 657

## Method 2: DECHEMA

This method uses a DECHEMA correlation of the Antoine equation. The equation is as follows

$$
\ln (P v p)=A-\frac{B}{T+C}
$$

Where $P v p=$ Vapour pressure, bars
$T=$ Temperature, K
The parameters required on the respective PPD_PropParam keyword are:

| Parameter <br> Number | Parameter <br> Name | Parameter Symbol |
| :---: | :--- | :--- |
| 1 | Antoine A | $A$ |
| 2 | Antoine B | $B$ |

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| 3 | Antoine C | $C$ |
| :--- | :--- | :--- |

Ref. The Properties of Gases and Liquids, 4th Edition, Reid, Prausnitz and Poling, p. 208

## Method 3: Modified Antoine (HYSYS)

This method uses a modified version of the Antoine equation, as used in the Hyprotech HYSYS simulator. The equation is:

$$
\ln (P v p)=A+\left(\frac{B}{T+C}\right)+D \ln (T)+E T^{F}
$$

Where Pvp = Vapour pressure, kPa
$T=$ Temperature, K
The parameters required on the respective PPD_PropParam keyword are:

| Parameter <br> Number | Parameter <br> Name | Parameter Symbol |
| :---: | :---: | :--- |
| 1 | Antoine A | $A$ |
| 2 | Antoine B | $B$ |
| 3 | Antoine C | $C$ |
| 4 | Antoine D | $D$ |
| 5 | Antoine E | $E$ |
| 6 | Antoine F | $F$ |

Ref. HYSYS User documentation v2.4.1

## Method 4: Modified Antoine (Aspen)

This method uses a modified version of the Antoine equation, as used in the Aspentech AspenPlus simulator. The equation is:

$$
\ln (P v p)=A+\left(\frac{B}{T+C}\right)+D T+E \ln (T)+F T^{G} \quad \text { for } \mathrm{T}_{\min } \leq T \leq \mathrm{T}_{\max }
$$

Where $P v p=$ Vapour pressure, bars
$T=$ Temperature, K
The parameters required on the respective PPD_PropParam keyword are:

| Parameter <br> Number | Parameter <br> Name | Parameter Symbol |
| :---: | :---: | :--- |
| 1 | Antoine A | $A$ |
| 2 | Antoine B | $B$ |
| 3 | Antoine C | $C$ |
| 4 | Antoine D | $D$ |
| 5 | Antoine E | $E$ |
| 6 | Antoine F | $F$ |
| 7 | Antoine G | $G$ |
| 8 | Tmin | Lower temperature limit (K) |
| 9 | Tmax | Upper temperature limit (K) |

Ref AspenTech User Guide V10.2, Physical Property Methods and Models, p3-84

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## Equation of State

## Method 1: Ideal Gas (Raoult's Law)

There are no additional parameters associated with the Ideal equation of state.

## Method 2: Peng-Robinson

There are no additional parameters associated with the Peng-Robinson equation of state.

## Method 3: Soave-Redlich-Kwong (SRK)

There are no additional parameters associated with the SRK equation of state.

## Method 4: Grayson-Streed

There are no additional parameters associated with the grayson-streed equation of state.

## Activity Models

Activity models use one or more matrices of binary parameters, and in the case of the UNIQUAC model, two further component specific parameters.

Because parameters are required for each component pair, rather than for each individual component, a separate keyword is used to supply the parameters.

## Method 1: Wilson

This method uses the standard Wilson equation to calculate activity coefficients. The form of the equation is:

$$
\ln \gamma_{i}=-\ln \left(\sum_{j}^{N} x_{j} \Lambda_{i j}\right)+1-\sum_{k}^{N} \frac{x_{k} \Lambda_{k i}}{\sum_{j}^{N} x_{j} \Lambda_{k j}}
$$

Where $\gamma_{i}=$ activity co-efficient for component $i$
$\Lambda_{i j}=V_{j} / V_{i} \exp \left(-a_{i j}\right) / R T$
$\mathrm{a}_{i j}=$ binary interaction parameters for component pair $i, j$
$\mathrm{V}_{i}=$ molar volume of pure liquid component $i$ in $\mathrm{m}^{3} / \mathrm{kgmol}$
The parameters required on the respective PPD_InterParam keyword are:

| Binary Matrix No. | Interaction Parameters |
| :---: | :---: |
| 1 | $\mathrm{a}_{i j}$ |

The parameters required on the respective PPD_PropParam keyword are:

| Parameter <br> Number | Parameter <br> Name | Parameter Symbol/Description |
| :---: | :---: | :--- |
| 1 | Mol. Vol. | Molar volume, $\mathrm{m}^{3} / \mathrm{kgmole}$ |

## Method 2: NRTL

This method uses the standard NRTL equation to calculate activity coefficients. The form of the equation is:

$$
\ln \gamma_{i}=\frac{\sum_{j}^{N} \tau_{j i} G_{j i j} x_{j}}{\sum_{k}^{N} G_{k i} x_{k}}+\sum_{j}^{N} \frac{x_{j} G_{i j}}{\sum_{k}^{N} G_{k j} x_{k}}\left(\tau_{i j}-\frac{\sum_{k}^{N} x_{k} \tau_{k j} G_{k j}}{\sum_{k}^{N} G_{k j} x_{k}}\right)
$$

Where $\gamma_{i}=$ activity co-efficient for component $i$
$\tau_{i j}=\mathrm{a}_{i j} / R T$
$G_{i j}=\exp \left(-\alpha_{i j} \tau_{i j}\right)$
$\mathrm{a}_{i j}, \alpha_{i j}=$ two pairs of binary interaction parameters for component pair $i, j\left(\alpha_{i j}=\right.$ $\left.\alpha_{j i}\right)$

The parameters required on the respective PPD_InterParam keyword are:

| Binary Matrix No. | Interaction Parameters |
| :---: | :---: |
| 1 | $\mathrm{a}_{i j}, \mathrm{a}_{j i}$ |
| 2 | $\alpha_{i j}, \alpha_{j i}$ |

Note that because $\alpha_{i j}=\alpha_{j i}$. The keyword entry for the $\alpha$ matrix should contain identical values for the two parameters, e.g.

PPD_InterParam $=77,170,2,0.295,0.295 \quad ; \alpha_{i j}$ and $\alpha_{j i}$ for $i=77, j=$ 170

## Method 3: UNIQUAC

This method uses the UNIQUAC equation to calculate activity coefficients. The form of the equation is:

$$
\ln \gamma_{i}=\ln \frac{\Phi_{i}}{x_{i}}+\frac{z}{2} q_{i} \ln \frac{\theta_{i}}{\Phi_{i}}+l_{i}-\frac{\Phi_{i}}{x_{i}} \sum_{j}^{N} x_{j} l_{j}-q_{i} \ln \left(\sum_{j}^{N} \theta_{j} \tau_{j i}\right)+q_{i}-q_{i} \sum_{j}^{N} \frac{\theta_{j} \tau_{i j}}{\sum_{k}^{N} \theta_{k} \tau_{k j}}
$$

Where

$$
\begin{aligned}
\Phi_{i} & =\frac{r_{i} x_{i}}{\sum_{k} r_{k} x_{k}} \\
\theta_{i} & =\frac{q_{i} x_{i}}{\sum_{k}^{N} q_{k} x_{k}} \\
\tau_{i j} & =\exp \left(\mathrm{a}_{i j} / R T\right) \\
r_{i} & =\text { molecular-size parameter for component } i \\
q_{i} & =\text { molecular-surface parameter for component } i
\end{aligned}
$$

The parameters required on the respective PPD_InterParam keyword are:

| Binary Matrix No. | Interaction Parameters |
| :---: | :---: |
| 1 | $\mathrm{a}_{i j}$ |

The parameters required on the respective PPD_PropParam keyword are:

| Parameter <br> Number | Parameter <br> Name | Parameter <br> Symbol/Description |
| :---: | :---: | :--- |
| 1 | $\mathrm{r}_{i}$ | $\mathrm{r}_{i}$ |
| 2 | $\mathrm{q}_{i}$ | $\mathrm{q}_{i}$ |

## Method 4: NRTL (AspenTech)

This method uses an extended version of the NRTL equation as used in the AspenTech AspenPlus simulator. The form of the equation is:

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$$
\ln \gamma_{i}=\frac{\sum_{j}^{N} \tau_{j i} G_{j i} x_{j}}{\sum_{k}^{N} G_{k i} x_{k}}+\sum_{j}^{N} \frac{x_{j} G_{i j}}{\sum_{k}^{N} G_{k j} x_{k}}\left(\tau_{i j}-\frac{\sum_{k}^{N} x_{k} \tau_{k j} G_{k j}}{\sum_{k}^{N} G_{k j} x_{k}}\right)
$$

Where $\gamma_{i}=$ activity co-efficient for component $i$
$\tau_{i j}=\mathrm{a}_{i j}+\left(\mathrm{b}_{i j} / T\right)+\mathrm{e}_{i j} \ln (T)+\mathrm{f}_{i j} T$
$G_{i j}=\exp \left(-\alpha_{i j} \tau_{i j}\right)$
$\alpha_{i j}=c_{i j}+\mathrm{d}_{i j}(T-273.15 \mathrm{~K})$
$\mathrm{a}_{i j}$ to $\mathrm{f}_{j i}=$ six pairs of binary interaction parameters for component pair $i, j\left(\mathrm{c}_{i j}=\right.$ $\mathrm{c}_{j i}$ and $\mathrm{d}_{i j}=\mathrm{d}_{j i}$ )

The parameters required on the respective PPD_InterParam keyword are:

| Binary Matrix No. | Parameter Name |
| :---: | :---: |
| 1 | $\mathrm{a}_{i j}, \mathrm{a}_{j i}$ |
| 2 | $\mathrm{~b}_{i j}, \mathrm{~b}_{j i}$ |
| 3 | $\mathrm{c}_{i j}, \mathrm{c}_{j i}$ |
| 4 | $\mathrm{~d}_{i j}, \mathrm{~d}_{j i}$ |
| 5 | $\mathrm{e}_{i j}, \mathrm{e}_{j i}$ |
| 6 | $\mathrm{f}_{i j}, \mathrm{f}_{j i}$ |

Note that because $\mathrm{c}_{i j}=\mathrm{c}_{j i}$ and $\mathrm{d}_{i j}=\mathrm{d}_{j i}$ the keyword entry for the c and d matrices should contain identical values for the two parameters, e.g.

PPD_InterParam $=77,170,3,140.3,140.3 \quad ; \mathrm{c}_{i j}$ and $\mathrm{c}_{j i}$ for $i=77, j=$
PPD_InterParam $=77,170,4,-254.5,-254.3 \quad ; \mathrm{d}_{i j}$ and $\mathrm{d}_{j i}$ for $i=77, j=$ 170

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## Additional data elements

This is optional data can be stored in the .CMP file that is only used by CmpEdit and is not used by the general physical properties calculation engines.

## Physical properties calculator

## Stream conditions

```
PPC_Z = <n>, <r1>
```

Profile pressure <n> is the component index <r1> is the component mole fraction PPC_FLOW = <r1>
$<\mathrm{r} 1>$ is the fluid flowrate (kmole/s)
PPC_P = <r1>
<r1> is pressure (bar)
PPC_T_K = <r1>
<r1> is the temperature (Kelvin)
PPC_H = <r1>
<r1> is the specific enthalpy ( $\mathrm{kJ} / \mathrm{kmole}$ )
PPC_S = <r1>
$<r 1>$ is the specific entropy (Kw/K)
PPC_VF = <r1>
<r1> is the vapour fraction
PPC_Property = <n>
$<\mathrm{n}>$ is the index of the property to be calculated
PPC_Range_BL = <r1>
<r1> range calculation lower bound
PPC_Range_BU = <r1>
<r1> range calculation upper bound

## Profile properties

```
PPC_ENV_T_Min_K = <r1>
PPC_ENV_T_Max_K = <r2>
PPC_ENV_Num_P = <n>
PPC_ENV_Num_Plot_Points = <n>
PPC_ENV_P = <n>, <r1>
<n> is the component index
<r1> is the profile pressure (bar)
```


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## Appendix B - Example File

The following shows an example file for a three component mixture, with four properties present.

## Components:

| i-butane | ID Number 259 |
| :--- | :--- |
| propane | ID Number 206 |
| i-pentane | ID Number 312 |
| n-pentane | ID Number 311 |
| n-butane | ID Number 258 |

## Properties

Enthalpy (ref. no. 2), using method 1 (Heat Capacity, Reid-Prausnitz-Poling)
Vapour Pressure (ref. no. 3), using method 1 (Reid-Prausnitz-Poling)
Equation of State (ref. no. 11), using method 1 (Ideal Gas)


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| PPD_Criticaldat2 | $=$ | 311, | 0.0000000 | . 0000000 |  | 0000000 |  | 0.0000000 |  | 0.0000000 |  | 0.0000000 |  | 0.0000000 |  | 00 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| , 0.0000000 |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| PPD_CriticalDat2 |  | 258, | 0.00 | 0.0000000 |  | 0.0000000 |  | 0.0000000 |  | 0.0000000 |  | 0.0000000 |  | 0.0000000 |  | 0.0000000 |

[\#\#\# Physical Property Parameters (Property, Component ID, Parameter Number, Value]
[\#\#\# Enthalpy parameters for in
PPD_PropParam $=\quad 2, \quad 259, \quad 1,-1.3900000$
PPD_PropParam $=\quad 2,259, \quad 2,0.38470000$
PPD PropParam $=\quad 2,259, \quad \begin{aligned} & 3,-0.18500000 E-03 \\ & 4, ~ 0.28950000 E-07\end{aligned}$
\#\#\# Enthalpy parameters for propane]
PPD_PropParam = 2, 206, 1, -4.2240000
PPD_PropParam = 2, 206, 2, 0.30630000
PPD_PropParam $=2,206, \quad 3,-0.15900000 \mathrm{E}-03$
PPD_PropParam $=2,206,4,0.32150000 \mathrm{E}-07$
[\#\#\# Enthalpy parameters for i-pentane]

[\#\#\# Enthalpy parameters for $n$-pentane]
PPD_PropParam $=\quad 2,311, \quad 1,-3.6260000$
PPD_PropParam $=2,311, \quad 2,0.48730000$
PPD PropParam $=\quad 2,311,4,-0.25800000 \mathrm{E}-03$
[\#\#\# Enthalpy parameters for $n$-butane]
PPD_PropParam = 2, 258, 1, 9.4870000
PPD_PropParam $=\quad 2,258,2, \quad 2,0.33130000$
PPD_PropParam $=\quad 2,258, \quad 3,-0.11100000 \mathrm{E}-03$

| \#\# Va | ure |  |  | tane] |
| :---: | :---: | :---: | :---: | :---: |
| PPD_PropParam | = | 3, 259, | 1, | 1.0000000 |
| PPD_PropParam |  | 3 , 259, | 2, | -6.9557900 |
| PPD_PropParam | = | 3 , 259, | 3, | 1.5009000 |
| PPD_PropParam | = | 3 259, | 4, | -2.5271700 |
| PPD_PropParam | = | 3 , 259, | 5, | -1.4977600 |
| PPD_PropParam | = | 3 3 259, | 6, | 165.000 |
| PPD_PropParam | = | 3,259, | 7, | 408.200 |

[\#\#\# Vapour Pressure parameters for propane]

| PPD_PropParam $=$ | 3,206, | $1,1.0000000$ |
| :--- | :--- | :--- |
| PPD PropParam $=$ | 3,206, | $2,-6.7221900$ |

PPD PropParam $=3,206,2,-6.7221900$
PPD PropParam $=3,206,4,-2.138680$
PPD_PropParam $=3,206,5,-1.385510$
PPD_PropParam $=$ 3, 206, 6, 145.0000

3, 206, 7, 369.8000
[\#\#\# Vapour Pressure parameters for i-pentane]

| PPD_PropParam $=$ | 3, | 312, | 1, |
| :--- | :--- | :--- | :--- |
| PPD_PropParam $=$ | 3, | 312, | 2, |
| P. | 127270000 |  |  |

PPD Propparam $=\quad 3,312,3,-7.1272700$
PPD_PropParam $=3,312,4,-2.543020$
PPD_PropParam $=3,312, \quad 5,-2.456570$
PPD_PropParam = 3, 312, 6, 220.0000
, 312, 7, 460.4000
[\#\#\# Vapour Pressure parameters for n-pentane]

| PPD_PropParam $=$ | 3,311, | $1,1.0000000$ |
| :--- | :--- | :--- |
| PPD PropParam $=$ | 3,311, | $2,-7.2893600$ |

PPDDPropParam $=3,311,3,-7.2893600$
PPD PropParam $=3,311,4,-3.083670$
PPD PropParam $=3,311,5,-1.024560$
PPD_PropParam $=3,311,6,195.0000$
PPD_PropParam $=$ 3, 311, 7, 469.70000
[\#\#\# Vapour Pressure parameters for n-butane]
PPD_PropParam $=\quad 3,258, \quad 1,1.0000000$
PPD Proparam $=3,258$ 3, 6.887990
PPD PropParam $=3,258,4,-1.998730$

PPD_PropParam $=3,258, \quad 5,-3.1300300$
PPD_PropParam $=$ 3, 258, 6, 170.0000
7, 425.2000
[\#\#\# Interaction Parameters]
\#\#\# (Component i ID, Component j ID, Parameter Array, $\operatorname{Array}(\mathrm{I}, \mathrm{J}), \operatorname{Array}(\mathrm{J}, \mathrm{I})$ ]
[\#\#\# Phys Prop Calculator]
 1824
The University of Manchester

